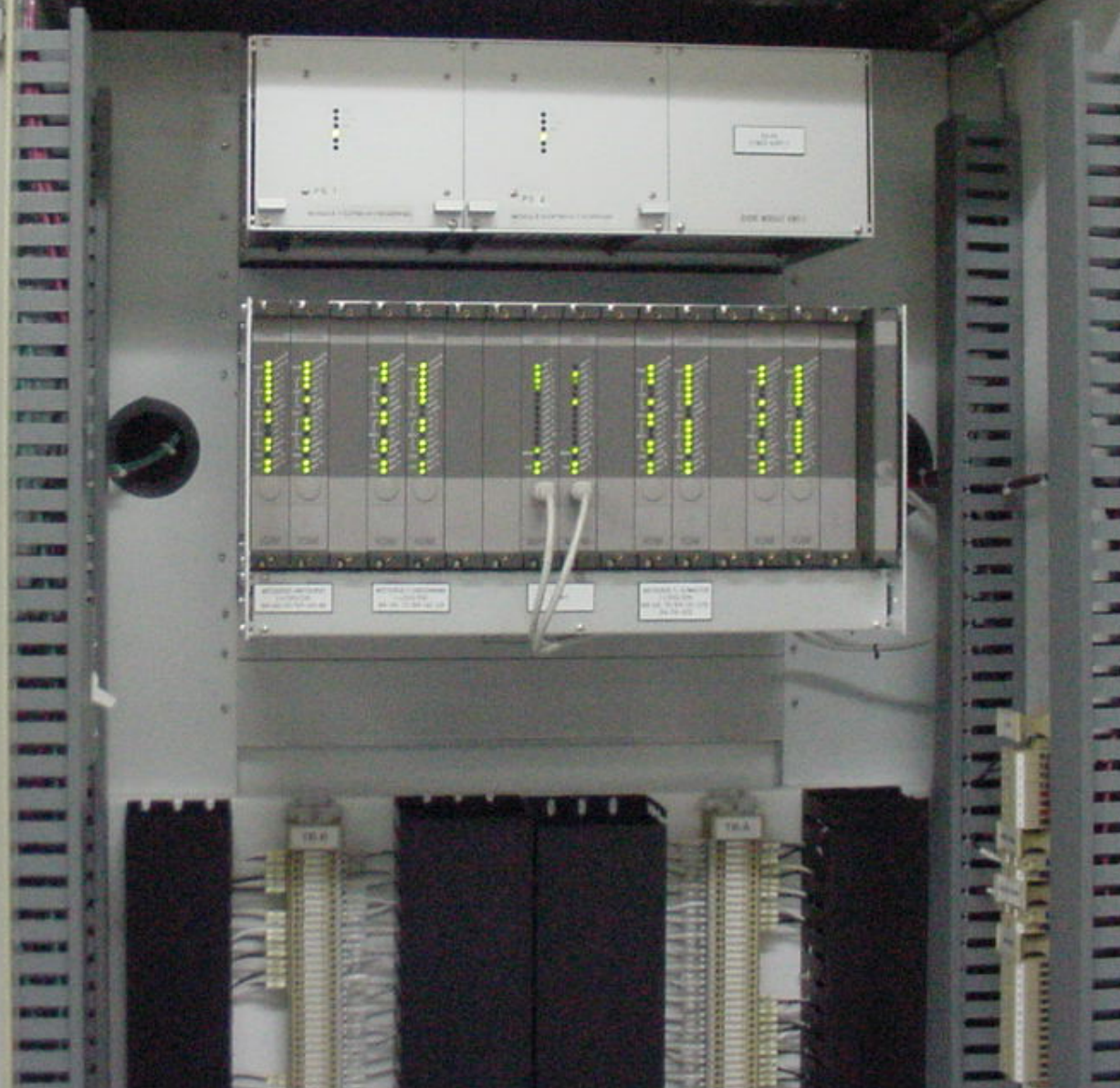


# CCC Overview

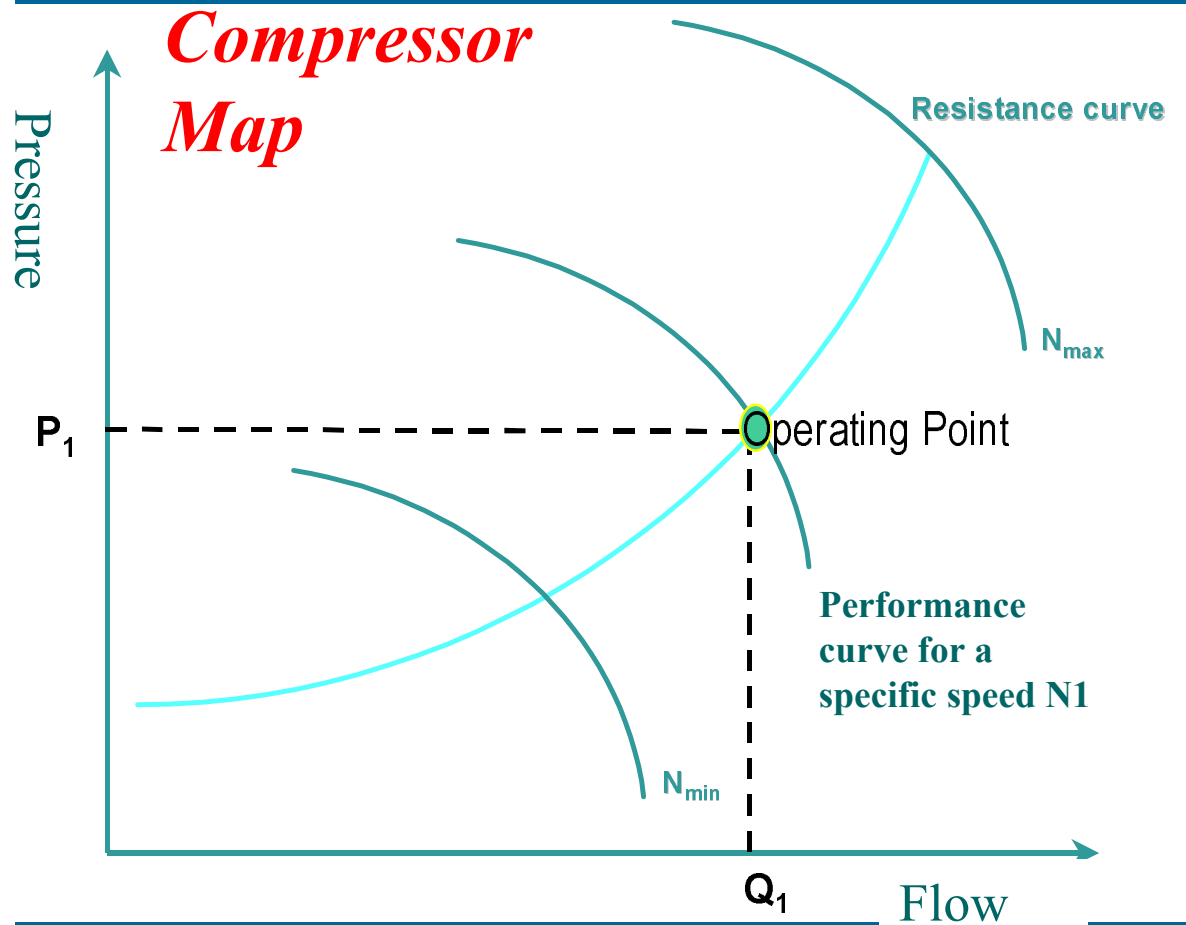
Dan  
McDougall



# Presentation Overview

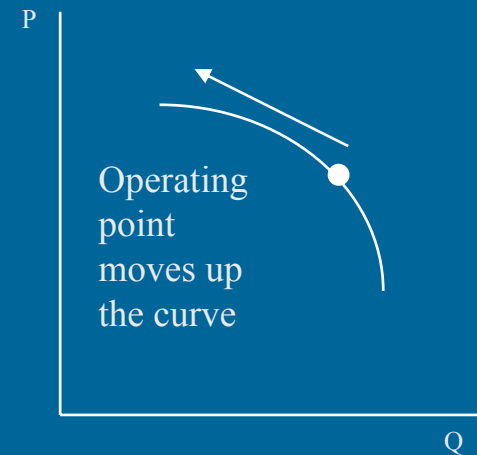
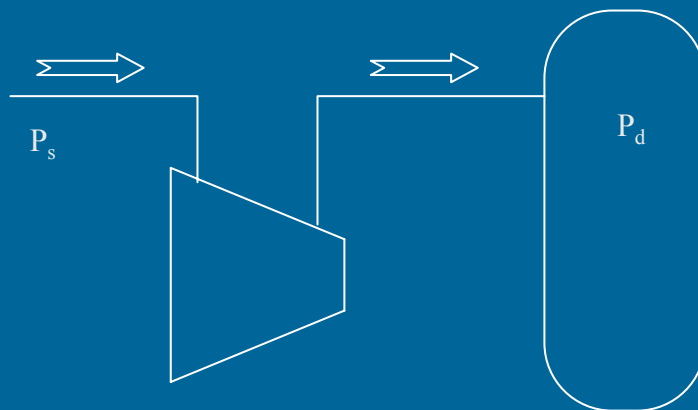
- What is surge?
- How does CCC control surge?
  - Deviation, Recycle Fast & Safety-On
- What is a Performance Controller?
  - Temp track & limit control
- CCC System Alarms

# What is surge?



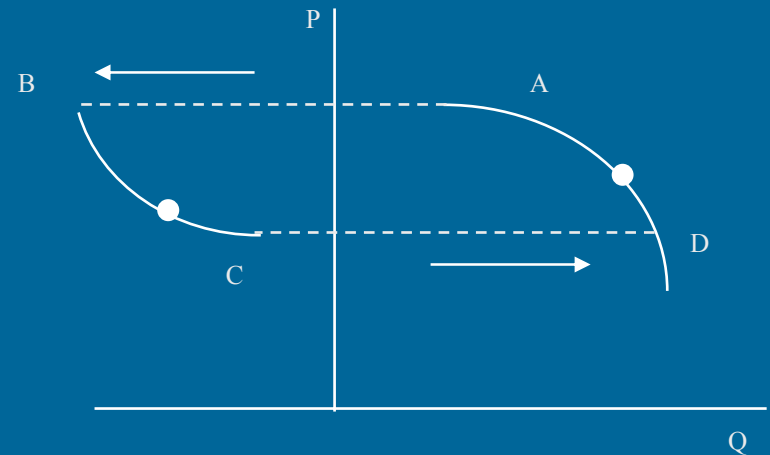
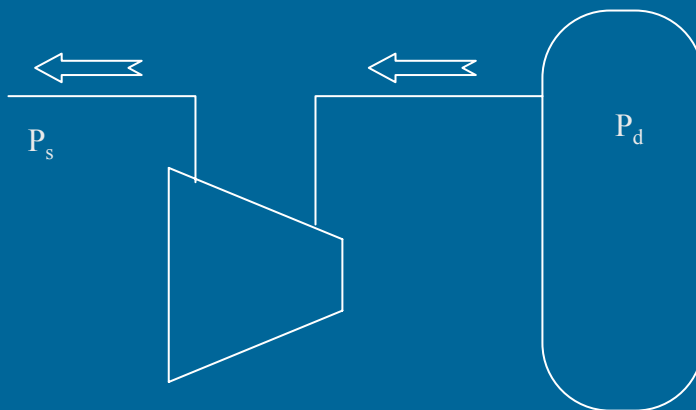
# What is surge?

- $P_d$  rises
- delta-P across compressor rises
- Compressor loses ability to make pressure



# What is surge?

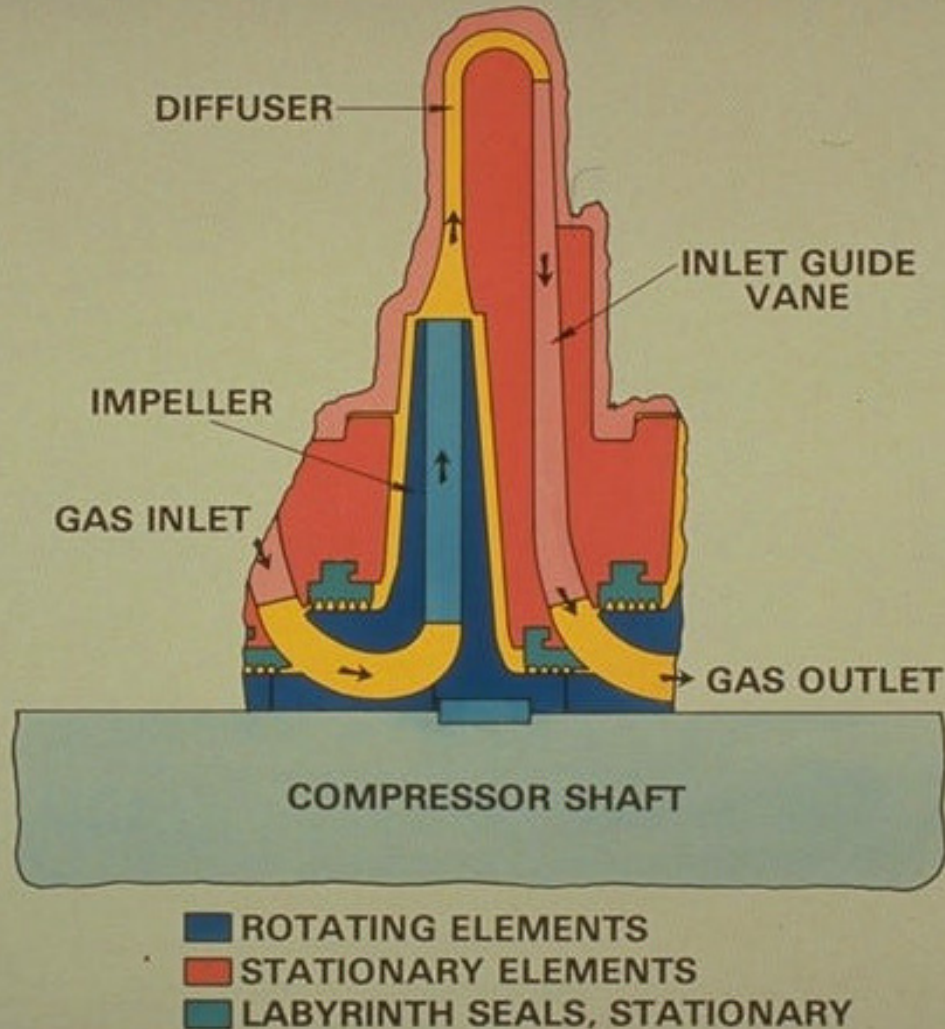
- Flow reverses
- $\Delta P$  across compressor drops
- Compressor moves back to stable region
- Cycle starts again...



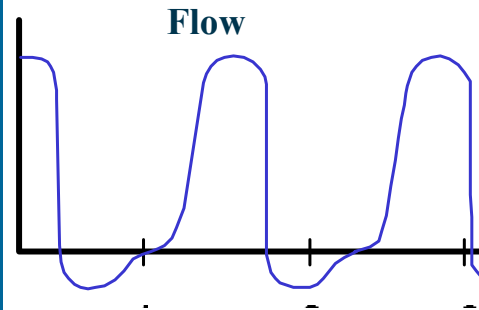
Operating point  
'jumps' from +ve and  
-ve flow

# What is surge?

TYPICAL COMPRESSOR STAGE



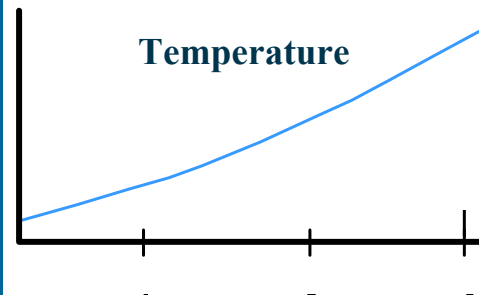
# What is surge?



- Rapid flow swings
- Thrust reversals



- Rapid pressure swings & instability



- Rising temps inside compressor

# What factors lead to surge?

- Start-up / Shutdown
- Reduced throughput
- Abnormal conditions

Trips

Power loss

Load changes

Cooler problems

Turbine problems

Operator error

Process Upsets

Gas composition changes

Filter / strainer problems

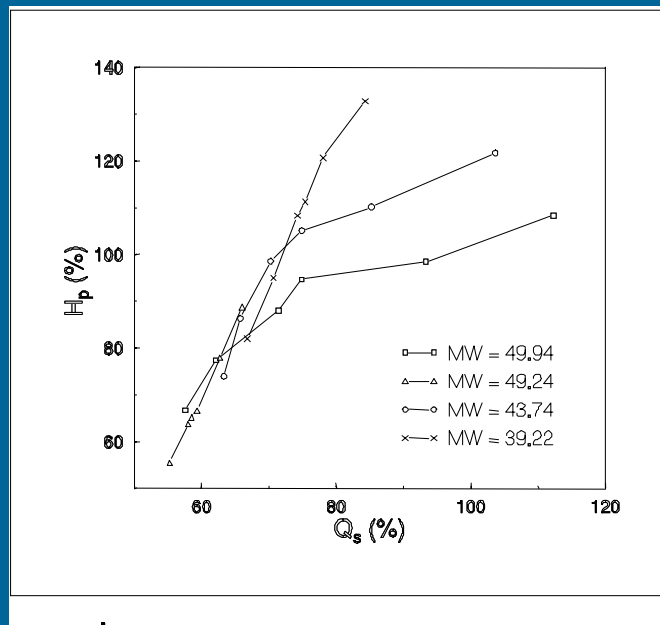


# How does CCC control surge?

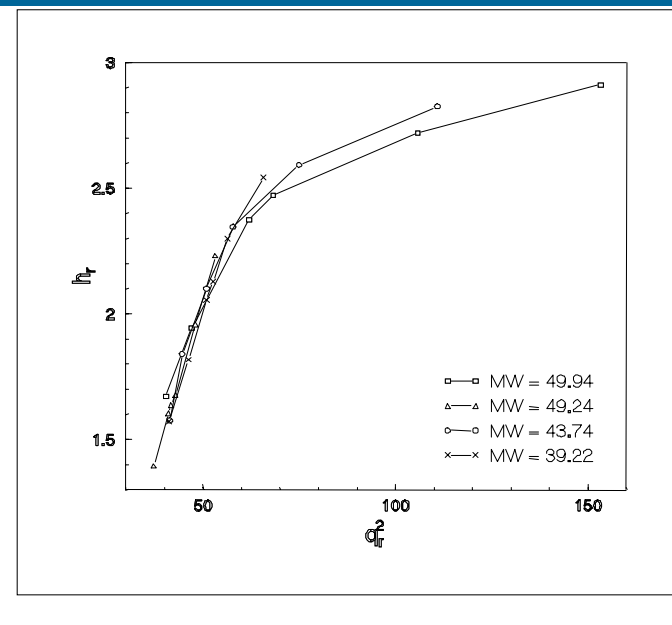
- The Challenge
  - Most efficient operating point is just before you reach surge. How do you measure your proximity to surge accurately so we can run as close as possible to the surge limit?
- The Solution
  - Invent a number called 'deviation' that is only dependent on flow / pressure / temperature

# How does CCC control surge?

Most OEM head-flow curves are dependent on many factors  
e.g. Molecular Weight



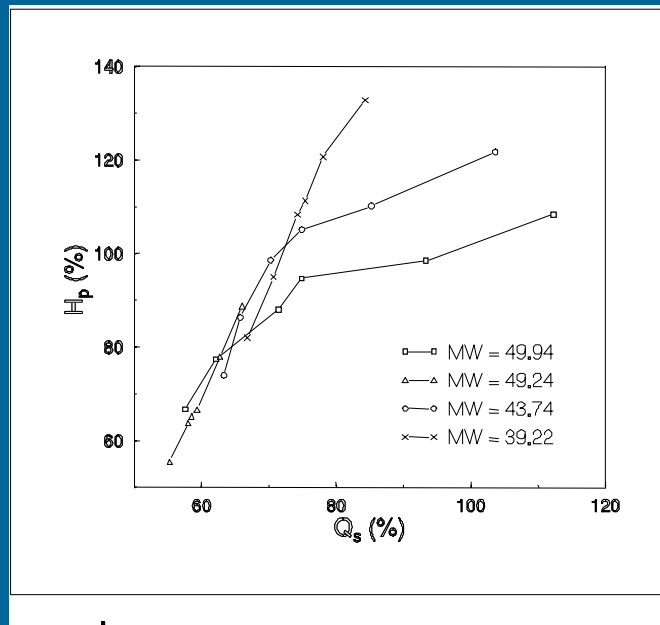
Vendor head-flow curves



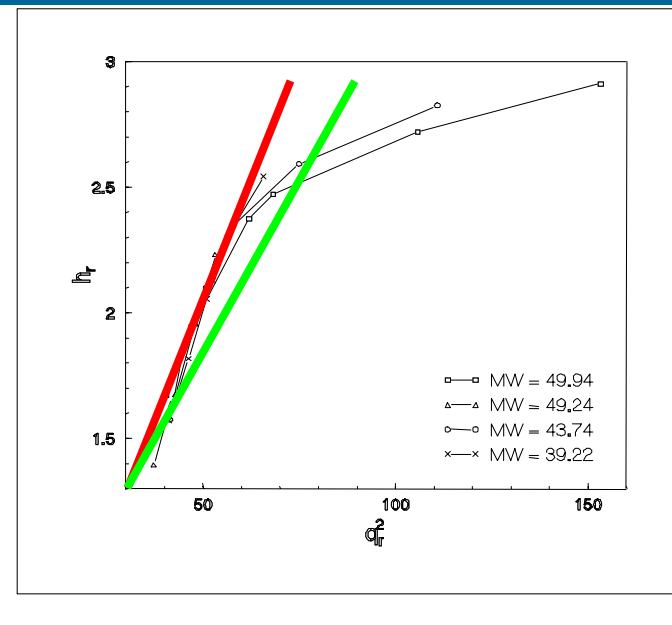
Reduced head-flow curves

# How does CCC control surge?

By using reduced (standardised) values the Surge-Limit-Line and Surge-Control-Line can be defined



Vendor head-flow curves



Reduced head-flow curves

# How does CCC control surge?

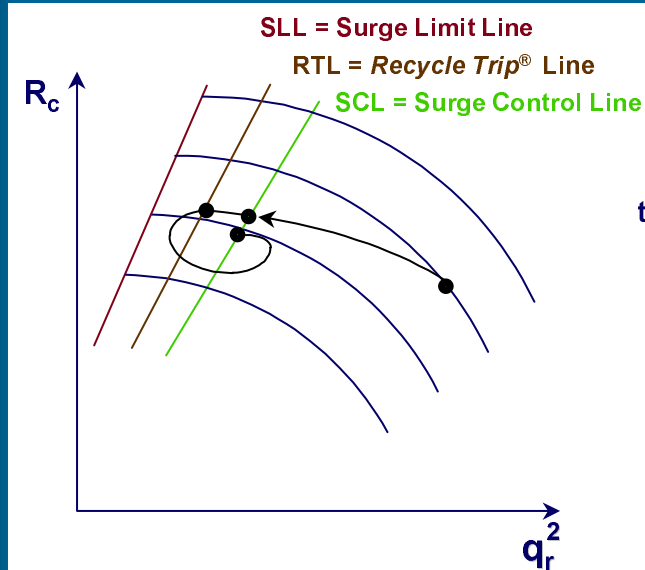
- DEVIATION
  - Arbitrary number that says how far from the Surge Control Line we are operating
  - Dev = 0 when on the control line
  - Dev = +ve when moving away from surge
  - Dev = -ve when moving towards surge
  - Ranged from -1 to +1

# How does CCC control surge?

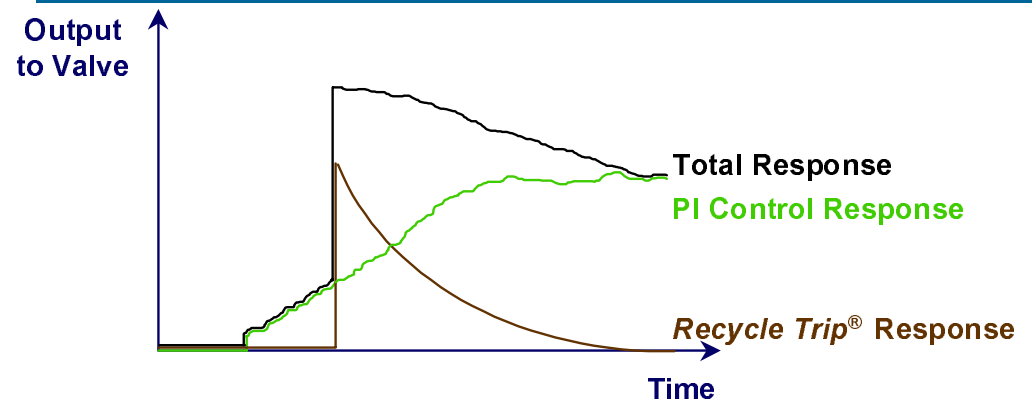
- Control Scheme
  - If  $Dev > 0$ , close recycle valve
  - If  $Dev < 0$ , open recycle valve
  - Normal PI control, just like any other loop

# How does CCC control surge?

- Recycle Fast
  - If deviation moves quickly towards surge, CCC gives the valve a 'kick'

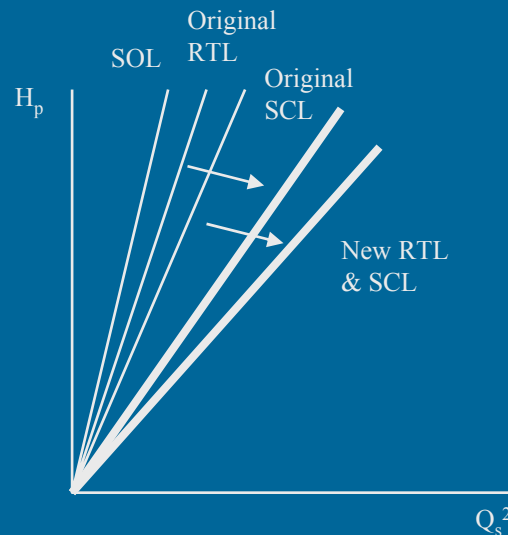


\* Holds the last value for 2.5 sec!



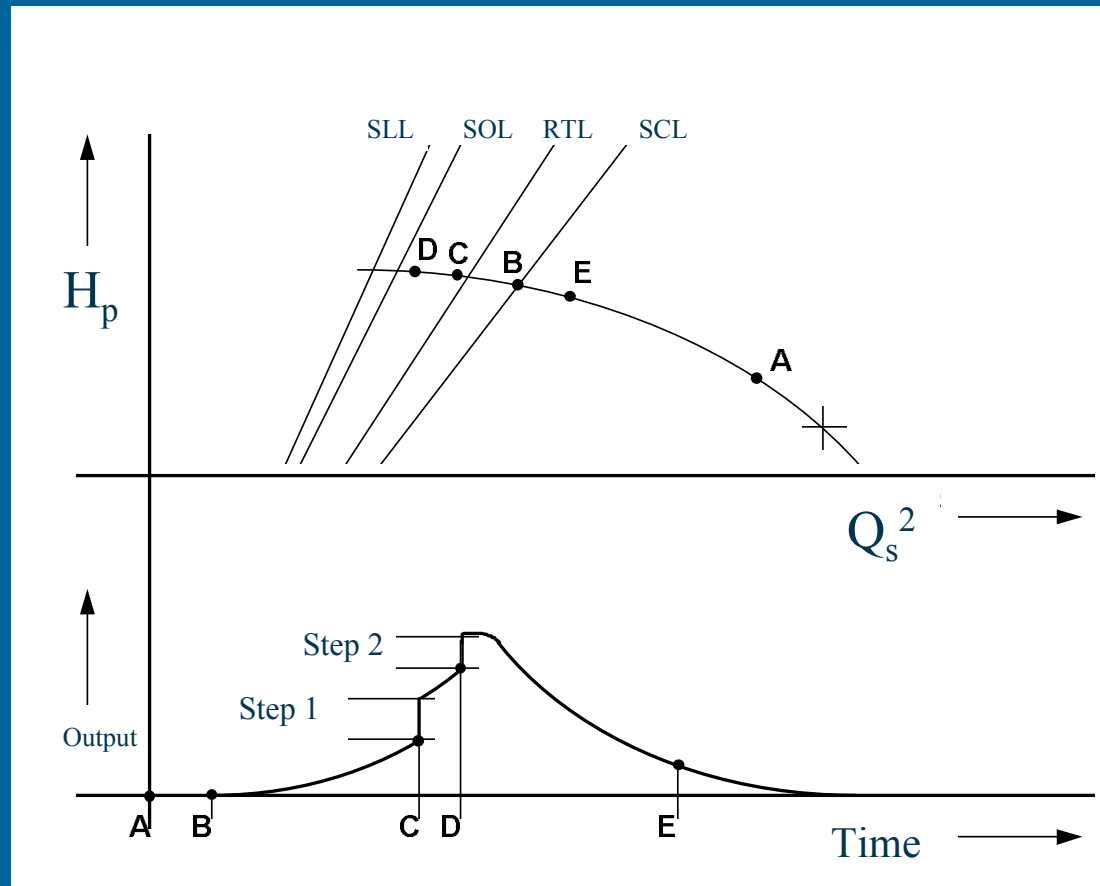
# How does CCC control surge?

- Safety-On
  - Compressor has surged or a very low deviation
  - *No additional valve response*
  - Moves the Surge Control Line further to the right



# How does CCC control surge?

- Typical response:

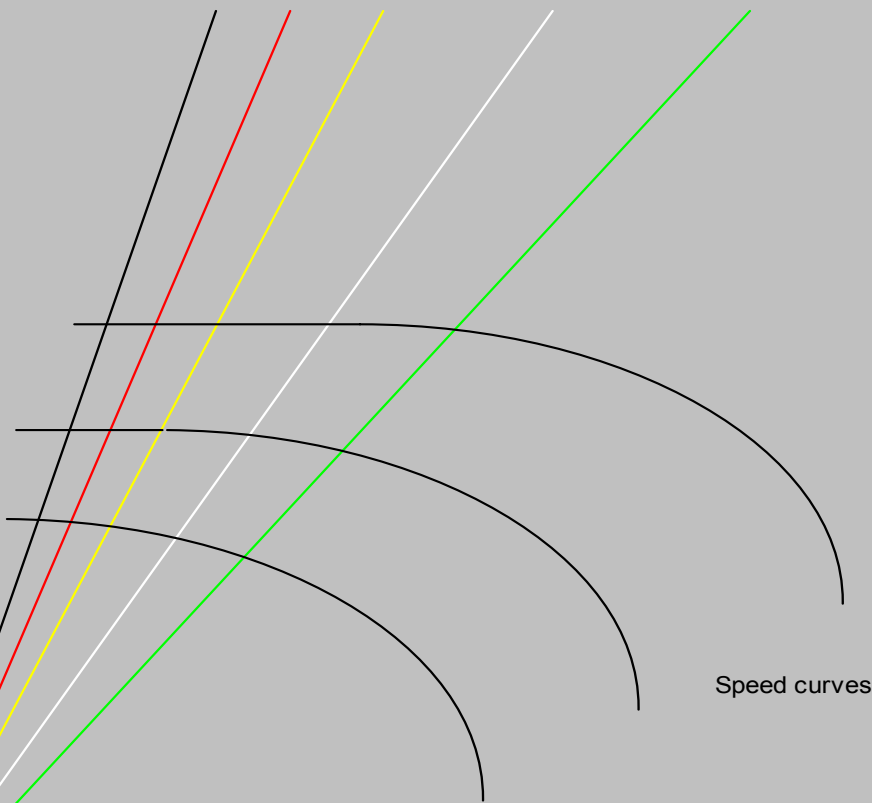




# CCC Control Points

1

(-0.4) (-0.2) (-0.1) (Dev = 0) (Dev = 0.15)  
STL SOL RTL SCL TSL



Speed curves

STL: Surge Trip Line  
SOL: Safety-On Line  
RTL: Recycle-trip Line  
SCL: Surge Control Line  
TSL: Tight Shut-off Line

0

0

1

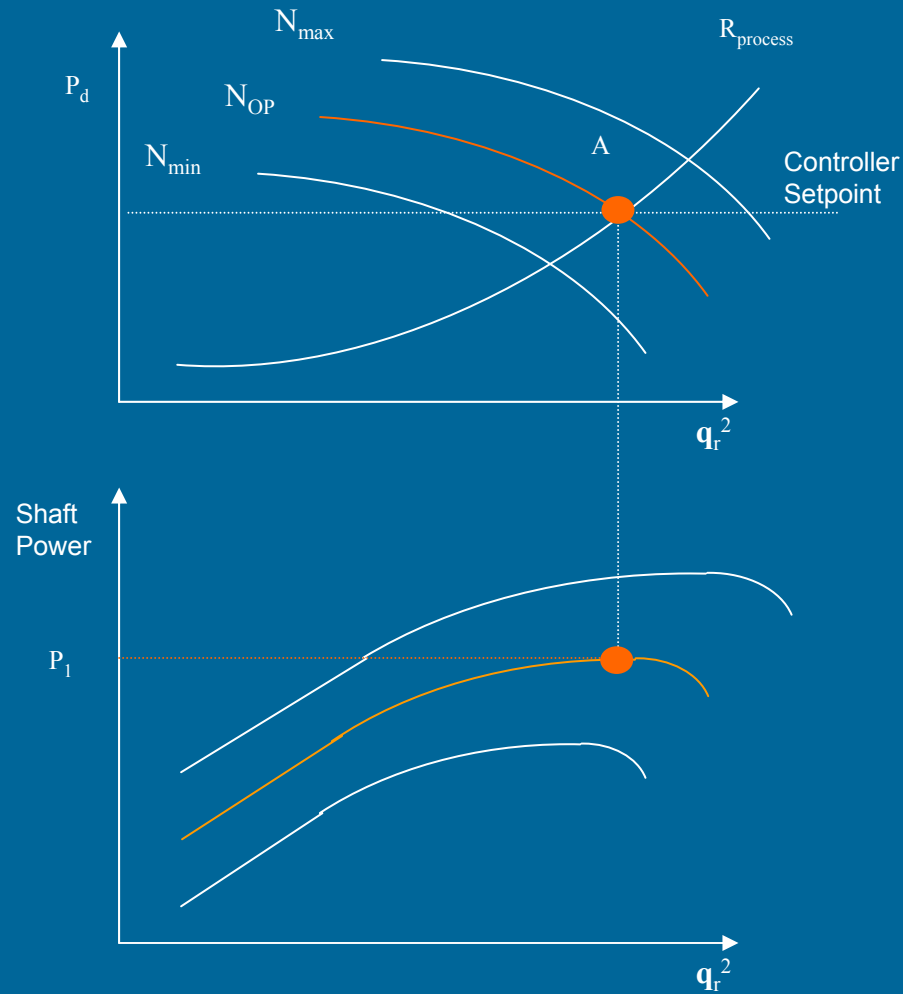
# CCC Control - Summary

- Tight-shutoff line (Dev ~ 0.15)
  - Valve is clamped down onto seat, low risk of surge
- Surge-Control line (Dev = 0)
  - PID control of valve at dev = 0
- Recycle-trip line (Dev ~ -0.1)
  - Steps open valve about 10 - 15%
  - Holds the valve for about 2.5s
  - Poor response of valve can lead to trip!!
- Safety-On line (Dev ~ -0.2)
  - Moves all lines to the right & increments surge count
  - Valve steps open due to PID response
- Surge Trip line (Dev ~ -0.4)
  - Would expect compressor to be surging
  - 3 surges in 6 seconds will trip compressor

# Performance Controller

- Used to control compressor throughput
  - blow-off
    - used more for plant air systems
  - discharge throttling
    - inefficient
  - suction throttling
    - often used on electric-drive compressors
  - compressor guide-vane control
    - efficient
  - speed variation
    - Used in Domgas & LNG

# Performance Controller

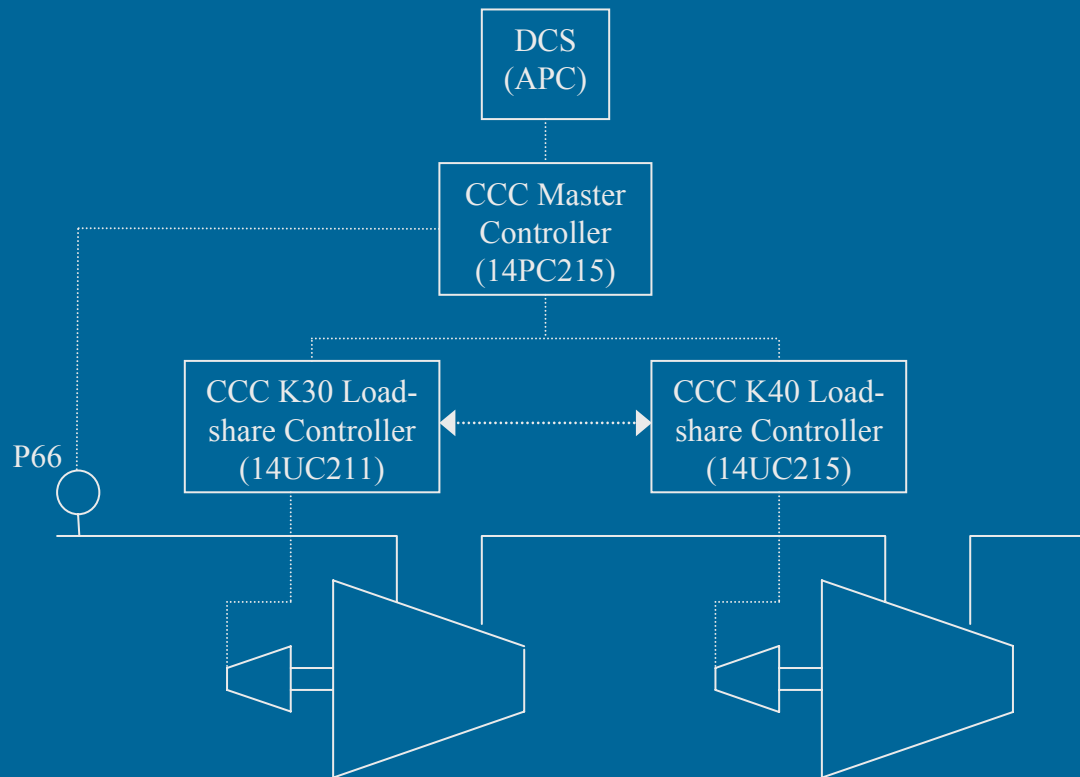


# Performance Controller

- Limit Control
  - Ensures a physical constraint is not exceeded.  
E.g:
    - Pd max of 2350kPa on K1440 discharge
- Temp tracking:
  - Mark IV or V may limit on EGT
  - CCC designed to ‘track’ speed
    - provides bumpless transfer back to CCC control
  - Historically, has provided problems
    - Incorrectly tuned

# Load Sharing

- Regulate capacity & maximise efficiency
- Provides control of a network



# Load Sharing

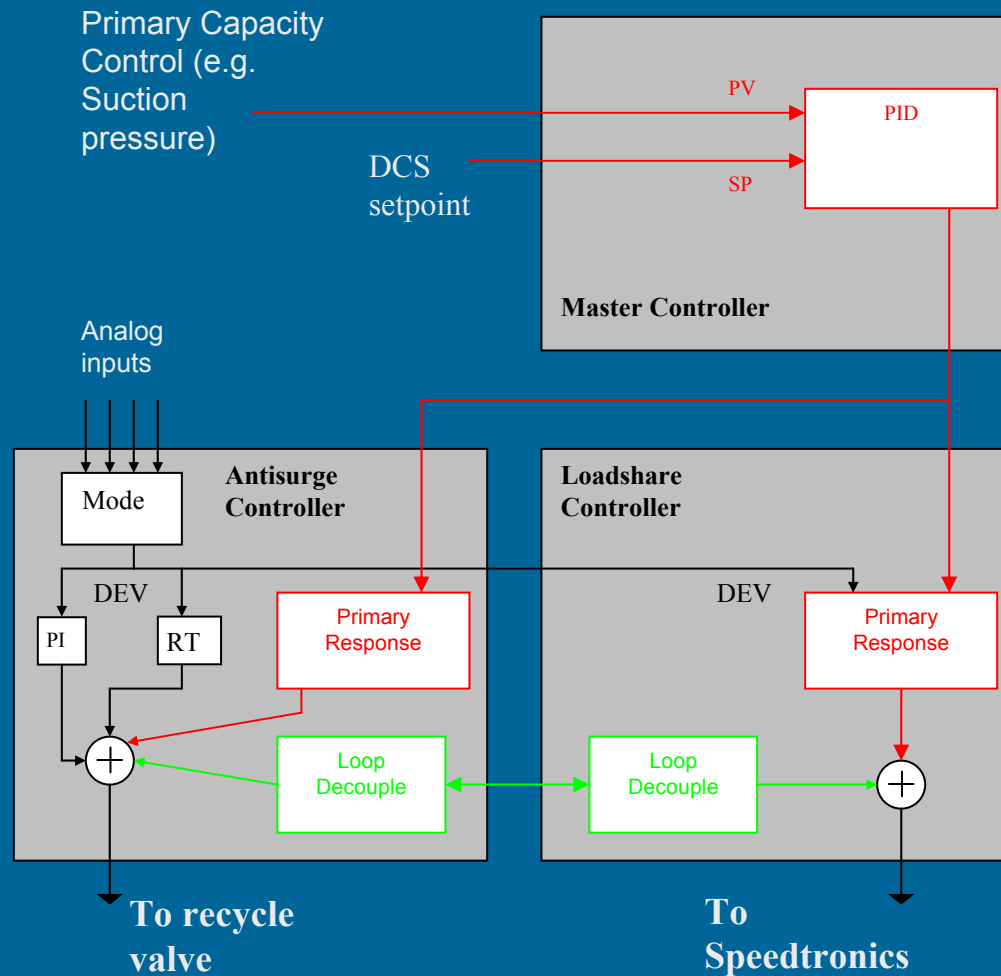
- Comprises of two types of response:
  - Primary Capacity Control
    - Manipulates a variable by adjusting speed / recycle
      - e.g. Suction pressure on K30
    - ‘visible’ load-sharing response
  - Load-balancing
    - Ensures both compressors operate in the same region
      - I.e. minimise un-necessary recycle
    - De-couples response of the anti-surge & performance controllers

# Load Balancing

- Equidistant control
  - Compressors in series
    - Equalise normalised compression ratio
    - Used on LNG MR and C3 circuits
  - Compressors in parallel
    - Equalise recycle deviation
    - Used on Domgas K30
    - Note: Domgas K20 load-sharing performed in DCS



# Loadsharing control scheme

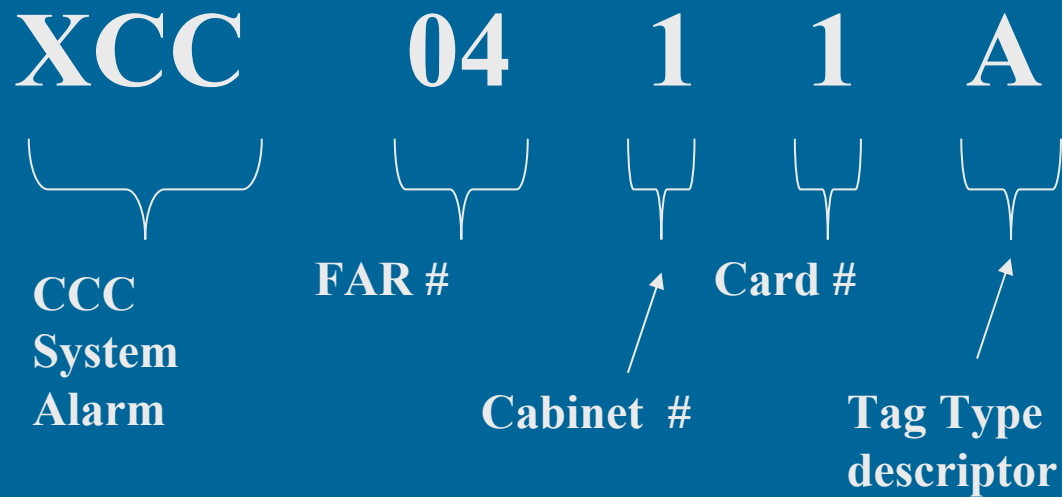


# CCC System Alarms

- Historically, not much information available on DCS
  - Application faults & hardware faults only
- New alarms utilise graphics to display origin of a fault
  - Any CCC alarm should be referred back to the graphic

# CCC System Alarms

- Tag convention



# How does CCC send alarms?

- Any event causes an alarm
  - Each alarm has a criticality and location
  - Hit the 'acknowledge' target on the graphic
    - If the alarm goes away, the fault has cleared
    - The criticality will remain until an Inlec has investigated
      - Most alarms require no further action apart from a workorder
    - New faults will now be able to initiate the alarm
  - Application faults have a 'look-up' table
  - Refer to the Control Instructions for more info!

# Fallback Alarm

- This alarm means CCC has lost the ability to control
  - e.g. lost both flow transmitters
- Response:
  - Recycle valve opened in manual to approx 50%
    - exact amount depends on the controller setting
      - minimum flow required to stay out of surge for all conditions
  - Performance controller goes to manual at last OP

10/1/02 10:09:47 AM 224-UIC-02 - Control Response At High Clamp  
 10/1/02 10:09:57 AM 224-UIC-02 - Control Response At High Clamp

CLEARED  
 ACTIVE

1FIC-014:PV	5808	2FIC-014:PV	5885	PIC-604:PV	4280
1FIC-014:SP	5808	2FIC-014:SP	5870	PIC-604:SP	3993

Control System | Trends | Maps | Archives | Events | Alarms | Config. | Print

info project

# Compressor 1-K-2420 & 1-K-2430

CCC# 6931  
 Compressor 1-K-2420/30  
 Compressor 2-K-2420/30

124-FIC-014 - Performance

Main Control: **Automatic**

PV 5808 TON/hr. Limit / POC  
 SP 5808 TON/hr. Remote  
 OUT 75.64 % Local  
 Status: Track Fallback  
 Track  
 Running

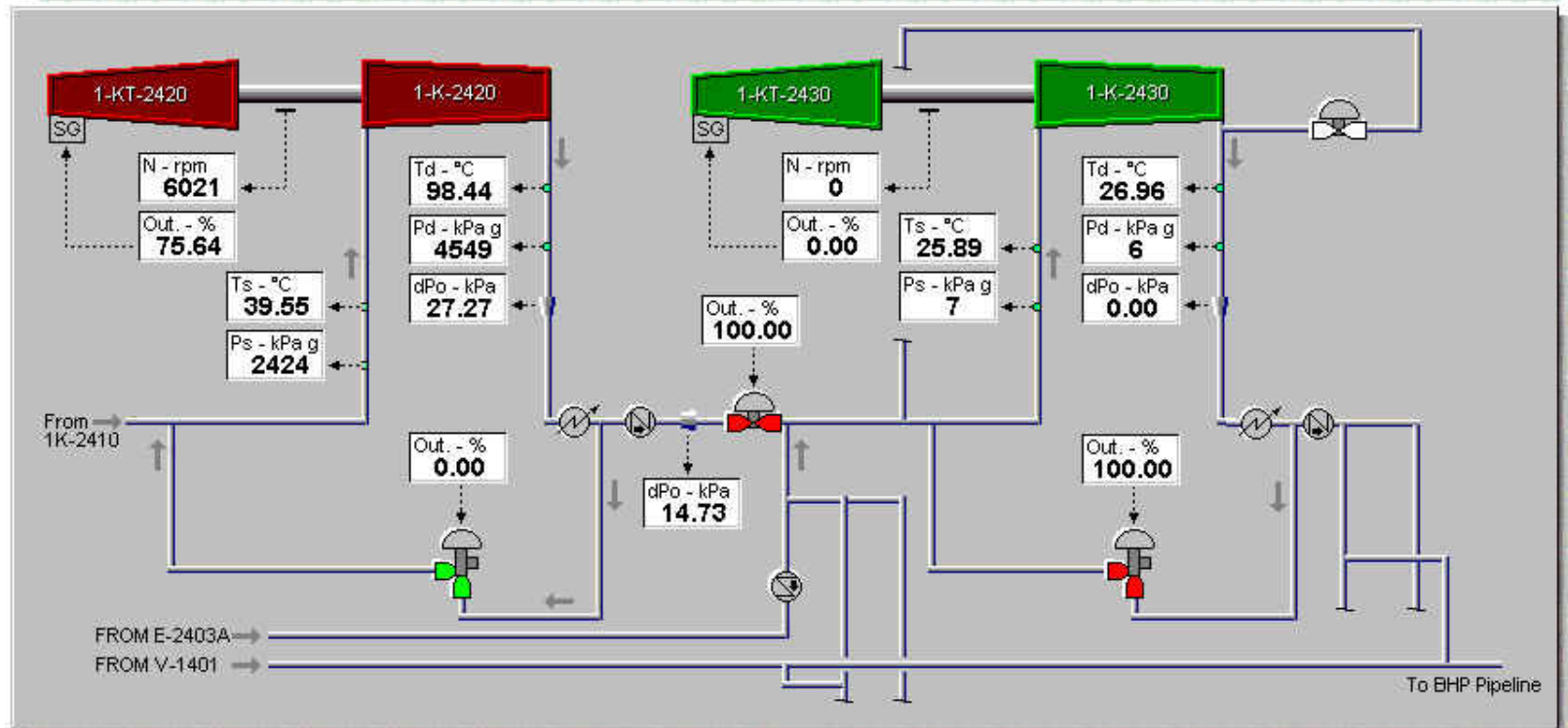
Auto Manual Remote Local

1 2 Reset Zoom Zoom hr / q2 Rc / q2 Rc / Qs Pd / Qst Trend

Calculated Variables

DEV - Antisurge DEVIation	0.476
Hp - Polytropic Head - kJ / kg	93
Qs - Suction Flow - ACMH	16501
Qst - Standard Flow - SCMh	394366
W - Measured Flow - kg / hr.	300220

Controllers: **FIC-014** UIC-16 UIC-160 PIC-604 UIC-02 UIC-26



Alarm ACK

10/1/02 10:08:54 AM 124-FIC-014 - Performance Controller Status	TRACKING	1FIC-014:PV 5797	2FIC-014:PV 5892	PIC-604:PV 4285
10/1/02 10:08:56 AM 224-UIC-02 - Control Response At High Clamp	ACTIVE	1FIC-014:SP 5797	2FIC-014:SP 5870	PIC-604:SP 3993

## 1-K-2420, 1-K-2430, 2-K-2420, and 2-K-2430 - Summary Alarms

info project  
 CCC# 6931  
 Alarm Summary

Date	Time	Status	Alarm Description	Down	Up	PrintAll	PrintVis	PrintSet	High Set	Low Set	Value	Prior	Ackn
9/17/02	2:22:29 PM		1-K - IOM#1 Card #1 WARNING Alarm Lvl.									4	2:22:35 PM
9/17/02	2:22:29 PM		1-K - IOM#1 Card #2 WARNING Alarm Lvl.									4	2:22:35 PM
9/19/02	9:44:38 AM		2-K - IOM#1 Card #1 WARNING Alarm Lvl.									4	2:21:53 PM
9/19/02	9:44:38 AM		2-K - IOM#1 Card #2 WARNING Alarm Lvl.									4	2:21:53 PM